

Claim 4, line 1, delete "claims 1-3" and insert

--claim 1--;

Claim 5, line 1, delete "claims 1-4" and insert

--claim 1--;

Claim 6, line 1, delete "claims 1-5" and insert

--claim 1--;

Claim 7, line 1, delete "claims 1-6" and insert

--claim 1--;

Claim 8, line 1, delete "claims 1-7" and insert

--claim 1--;

Claim 9, line 1, delete "claims 1-8" and insert

--claim 1--;

Claim 10, line 1, delete "claims 1-9" and insert

--claim 1--;

Claim 11, line 1, delete "claims 1-10" and insert

--claim 1--;

Claim 12, line 1, delete "claims 1-11" and insert

--claim 1--;

Claim 13, line 1, delete "claims 1-12" and insert

--claim 1--;

Claim 14, line 1, delete "claims 1-13" and insert

--claim 1--;

Claim 15, line 1, delete "claims 1-14" and insert

--claim 1--; and

Claim 16, line 4, delete "claims 1-15" and insert

--claim 1--.

Please add the following new claim 17:

1 17. Process according to claim 2, wherein:  
2 the degree of dispersion is increased after the  
3 regeneration;  
4 the acid impregnated catalyst is reduced in a flow of  
5 hydrogen gas;  
6 the acid impregnated catalyst is oxidised in a flow of dry  
7 (<0.1 vol.% of water) air, followed by reduction;  
8 the reduction and or oxidising step are carried out at a  
9 temperature of between 250 and 600°C;  
10 the silica-alumina support has been prepared using a sol-  
11 gel method;  
12 the support has an Si-Al atomic ratio of from 0.1 to 300;  
13 the catalyst has a precious metal content of from 0.01 to 5  
14 wt.%, calculated on the basis of the weight of reduced catalyst;  
15 the catalyst is impregnated with an aqueous solution of the  
16 acid;

17 the acid is selected from the group of HCl, H<sub>3</sub>PO<sub>4</sub>, H<sub>2</sub>SO<sub>4</sub>  
18 HNO<sub>3</sub>, HBr and combinations thereof;

19 the amount of acid calculated on the basis of a ratio of  
20 equivalents of acid to atoms of precious metal is between 0.1  
21 and 100, preferably between 0.5 and 10;

22 prior to the impregnation, carbonaceous deposits on the  
23 catalyst are burned off;

24 the regeneration is carried out in a reactor, separate from  
25 the reactor in which the catalyst is used; and

26 the catalyst is a used catalyst from a process in the group  
27 consisting of hydrogenation, hydro-isomerisation, hydro-  
28 desulfurisation, hydrodewaxing and catalytic reforming.

1 18. Process for hydrogenation, hydro-isomerisation, hydro-  
2 desulfurisation or hydrodewaxing, comprising treating the  
3 feedstock in the presence of a catalyst that has been  
4 regenerated using the process of claim 17.

#### REMARKS

This Preliminary Amendment puts the claims into proper form for examination. Kindly calculate the filing fee based on the amended claims.